

Turbulence III.

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Turbulence modelling III.

Miklós Balogh

Budapest University of Technology and Economics Department of Fluid Mechanics

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Wall boundary conditions

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LES

Concept Filtering BC-s

- Both k and ε or ω require boundary conditions at the walls
- Before introducing the boundary conditions and the approximate boundary treatment techniques, some theory about wall boundary layers is required.

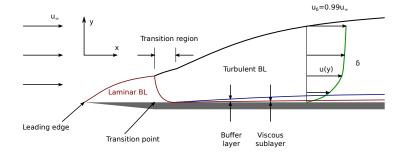


Boundary Layer

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Channel flow

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Characteristics

Flow between two infinite plates ⇒ fully developed

ullet Channel half width: δ

• Bulk velocity: $U_b \stackrel{\mathsf{def}}{=} \frac{1}{\delta} \int_0^\delta \overline{u} \, \mathrm{d} y$

• Bulk Reynolds number: $Re_b \stackrel{\mathrm{def}}{=} \frac{U_b 2 \delta}{\nu}$

• $Re_b > 1800$ means turbulence



Channel flow (contd.)

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Concept Filtering Streamwise averaged momentum equation:

$$0 = \underbrace{\nu \mathsf{d}_{y^2}^2 \overline{u}}_{\mathsf{d}_y \tau_l} - \underbrace{\mathsf{d}_y \overline{u'v'}}_{\mathsf{d}_y \tau_t} - \frac{1}{\rho} \partial_x \overline{p} \tag{1}$$

The pressure gradient $(d_x \overline{p_w})$ is balanced by the two shear stresses: $\tau = \tau_l + \tau_t$ Its distribution is linear:

$$\tau(y) = \tau_w \left(1 - \frac{y}{\delta} \right) \tag{2}$$



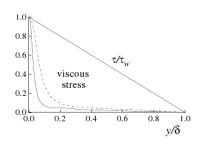
Channel flow (contd.) Two type of shear stresses

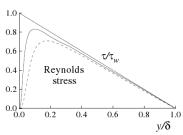
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The two shear stresses

- The viscous stress is dominant at the wall
- Turbulent stress is dominant far from the wall
- Both stresses are important in an intermediate region



Two scales of the flow at the wall

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Definitions

- Friction velocity: $u_{\tau} \stackrel{\text{def}}{=} \sqrt{\frac{\tau_w}{\rho}} = \sqrt{-\frac{\delta}{\rho}} \mathsf{d}_x \overline{p_w}$
- Friction Reynolds number: $Re_{\tau} \stackrel{\text{def}}{=} \frac{u_{\tau}\delta}{\nu} = \frac{\delta}{\delta_{\nu}}$
- Viscous length scale: $\delta_{\nu} \stackrel{\text{def}}{=} \frac{\nu}{u_{\tau}}$

General law of the wall can be characterised:

$$\mathsf{d}_y \overline{u} = \frac{u_\tau}{y} \varPhi\left(\frac{y}{\delta_\nu}, \frac{y}{\delta}\right) \tag{3}$$

 Φ is a function to be determined!





Law of the wall In wall proximity

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It can be assumed that only the wall scale plays a role in the near wall region:

$$d_y \overline{u} = \frac{u_\tau}{y} \Phi_I \left(\frac{y}{\delta_\nu} \right) \qquad \text{for } y \ll \delta$$
 (4)

Wall non-dimensionalisation \Box^+

$$u^{+} \stackrel{\text{def}}{=} \frac{\overline{u}}{u_{\tau}}$$
 (5)
$$y^{+} \stackrel{\text{def}}{=} \frac{y}{\delta_{\nu}} = \frac{yu_{\tau}}{\nu}$$
 (6)

$$y^{+} \stackrel{\text{def}}{=} \frac{y}{\delta} = \frac{yu_{\tau}}{v} \tag{6}$$



Határréteg sebességmegoszlása

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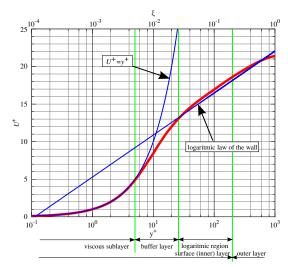
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Law of the wall Velocity

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Viscous sub-layer

- ullet Only au_l counts
- $u^+ = y^+$
- for $y^+ < 5$

Logarithmic layer

- Viscosity is not in the scaling
- $\Phi_I = \frac{1}{\kappa}$ for $y \ll \delta$ and $y^+ \gg 1$
- Log-law: $u^+ = \frac{1}{5} \ln(y^+) + B$
 - From measurements: $\kappa \approx 0.41$ and $B \approx 5.2$



Law of the wall Velocity

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Outer layer

- Φ depends only on y/δ
- In CFD we want to compute it for the specific cases! \Rightarrow We do not deal with it.



Reynolds stress tensor at the wall u_{τ} scaling

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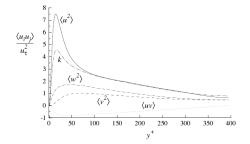
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Sharp peaks around $y^+ = 20$



Reynolds stress tensor at the wall k scaling

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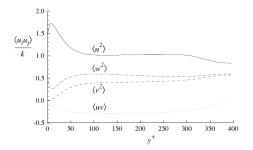
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A platau is visible in the log law region.

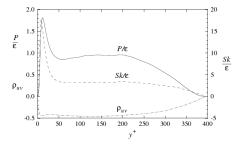


TKE budget at the wall

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- $\mathcal{P}/\varepsilon \approx 1$ in the log-law region
- $\mathcal{P}/\varepsilon \approx 1.8$ close to the wall



TKE budget at the wall

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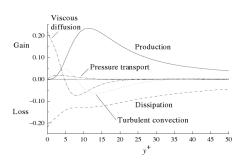
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- Turbulence is mainly produced in the buffer region $(5 < y^+ < 30)$
- Turbulence is viscous diffused to the wall
- Turbulence is strongly dissipated at the wall
- Conclusion: $\varepsilon = \nu d_{y^2}^2 u$ 0 y = 0



Numerical treatment of the wall layer, actual BC's Low Re treatment

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Concep Filterin In this treatment the complete boundary layer is resolved numerically

When to do?

- Low Reynolds number flow, where resolution is feasible
- If boundary layer is not simple, can not be described by law of the wall

How to do?

- Use a turbulence model incorporating near wall viscous effects
- Use appropriate wall resolution ($y^+ < 1$)



Numerical treatment of the wall layer, actual BC's High Re treatment

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Concep Filtering BC-s In this treatment the first cell incorporates the law of the wall

When to do?

- High Reynolds number flow, where it is impossible to resolve the near wall region
- If boundary layer is simple, can be well described by law of the wall

How to do?

- Use a turbulence models containing law of the wall BC
- Use appropriate wall resolution ($30 < y^+ < 300$)



Wall functions for RANS in practice (U, ν_t)

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Velocity at the wall:

- Dirichlet BC, no slip: U(y=0)=0
- Turbulent viscosity (for the wall adjacent cells):
 - Wall shear-stress (friction velocity) by definition:

$$\tau_w = u_\tau^2 = \nu_t \frac{\partial U}{\partial y}$$

• Laminar case $(y^+ \le y_{lam}^+)$:

$$U^+ = y^+ \to \nu_t = 0$$

• Turbulent case $(y^+ > y_{lam}^+)$:

$$U^{+} = \kappa \ln \left(Ey^{+} \right) \rightarrow \nu_{t} = \nu \left(\frac{\kappa y^{+}}{\ln \left(Ey^{+} \right)} - 1 \right)$$



Wall functions for RANS in practice (k, ϵ, P_k)

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Concep Filtering Turbulent kinetic energy (for the wall):

• Neumann BC: $\frac{\partial k}{\partial y} = 0$

- Turbulent kinetic energy dissipation (for the wall adjacent cells):
 - Equilibrium assumption:

$$P_k = \nu_t \left(\frac{\partial U}{\partial y}\right)^2 = C_\mu \frac{k^2}{\epsilon} \left(\frac{\partial U}{\partial y}\right)^2 = \epsilon$$

• Implementation:

$$\epsilon = \frac{C_\mu^{0.75} k^{1.5}}{\kappa y} \text{ and } P_k = (\nu + \nu_t) \left| \frac{\partial U}{\partial y} \right| \frac{C_\mu^{0.25} k^{0.5}}{\kappa y}$$



Numerical treatment of the wall layer, actual BC's Clever laws

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Concep Filtering The mixture of the two methods is developed:

- to enable the engineer not to deal with the wall resolution
- usually the mixture of the two method is needed, depending on actual position in the domain

Resolution requirements

At any kind of treatment the boundary layer thickness (δ) has to resolved by ≈ 20 cells to ensure accuracy.

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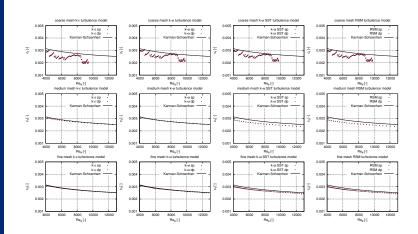
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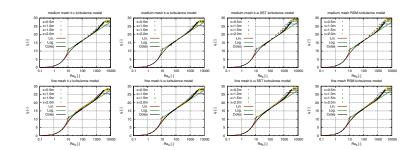
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Large-Eddy Simulation Difference between modelling and simulation

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Simulation

In the simulation the turbulence phenomena is actually resolved by a numerical technique, by solving the describing equations

Modelling

In the modelling of turbulence the effects of turbulence are modelled relying on theoretical and experimental knowledge. In the computation a reduced description of turbulence is carried out



Direct Numerical Simulation = DNS

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Concept Filtering BC-s The NS equations (describing completely the turbulence phenomena) are solved numerically

Difficulties

- The scales where the dissipation is effective are very small
 - The size of the smallest scales are Reynolds number dependent
- Simulation is only possible for academic situations (e.g.: HIT on 64 $\cdot 10^9$ cells)

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Concept of LES

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Concept

Compromise between RANS and DNS

- RANS: feasible but inaccurate
- DNS: accurate but infeasible

The large scales are import to simulate

- The large scales of the turbulent flow are boundary condition dependent, they needs to be simulated
- The small scales of turbulence are more or less universal and can be modelled 'easily'
- The removal of the small scales form the simulation reduce the computational cost remarkably



Filtering

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Filtering

How to develop the equations? How to separate between large and small scales?

Spatial filtering, smoothing using a kernel function

$$\langle \varphi \rangle (x_j, t) \stackrel{\mathsf{def}}{=} \int_V G_{\Delta}(r_i; x_j) \quad \varphi(x_j - r_i, t) \mathsf{d}r_i$$
 (7)



Filtering kernel

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Concept Filtering • G_{Λ} is the filtering kernel with a typical size of Δ .

- G_{Δ} has a compact support (its definition set where the value is non-zero is closed) in its first variable
- To be the filtered value of a constant itself it has to be true:

$$\int_{V} G_{\Delta}(r_i; x_j) dr_i = 1$$
 (8)

• If $G_{\Delta}(r_i;x_j)$ is homogeneous in its second variable and isotropic in its first variable than $G_{\Delta}(|r_i|)$ is a function of only one variable

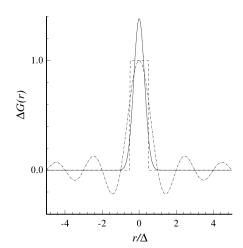


Filtering kernel Examples

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Filtering Physical space

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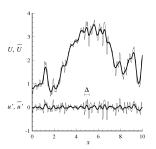
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Fluctuation:

$$\widetilde{\varphi} \stackrel{\text{def}}{=} \varphi - \langle \varphi \rangle \tag{9}$$

 $\langle \widetilde{\varphi} \rangle \neq 0$, a difference compared to Reynolds averaging



Filtering Spectral space

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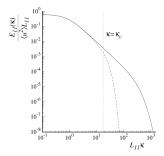
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Recall: the cutting wavenumber (κ_c) , below which modelling is needed

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Filtered equations

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• If using the previously defined (homogeneous, isotropic) filter

Averaging and the derivatives commute (exchangeable)

$$\partial_{i} \langle u_{i} \rangle = 0$$

$$\partial_{t} \langle u_{i} \rangle + \langle u_{j} \rangle \partial_{j} \langle u_{i} \rangle = -\frac{1}{\rho} \langle p \rangle + \nu \partial_{j} \partial_{j} \langle u_{i} \rangle - \partial_{j} \tau_{ij}$$
(10)

- 3D (because turbulence is 3D)
- unsteady (because the large eddies are unsteady)





Sub Grid Scale stress

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 τ_{ij} is called Sub-Grid Scale stress SGS from the times when filtering was directly associated to the grid

$$\tau_{ij} \stackrel{\text{def}}{=} \langle u_i u_j \rangle - \langle u_i \rangle \langle u_j \rangle \tag{12}$$

- It represents the effect of the filtered scales
- It is in a form a stress tensor
- Should be dissipative to represent the dissipation on the filtered small scale



Eddy viscosity model

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Filtering BC-s Same as in RANS

•

$$\tau_{ij} - \frac{1}{3}\tau_{kk}\delta_{ij} = -2\nu_t \langle s_{ij} \rangle \tag{13}$$

- Relatively a better approach since the small scales are more universal
- Dissipative if $\nu_t > 0$.



Smagorinsky model

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•

$$\nu_t = (C_s \Delta)^2 |\langle S \rangle| \tag{14}$$

$$|\langle S \rangle| \stackrel{\text{def}}{=} \sqrt{2s_{ij}s_{ij}}$$
 (15)

- C_s Smagorinsky constant to b determined
 - using spectral theory of turbulence
 - using validations on real flow computations
- Δ to be prescribed
 - Determine the computational cost (if too small)
 - Determine the accuracy (if too big)
 - 80% of the energy is resolved is a compromise



Scale Similarity model

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Let us assume that the cuted small scales are similar to the kept large scales!

A logical model:

$$\tau_{ij} \stackrel{\text{def}}{=} \left\langle \left\langle u_i \right\rangle \left\langle u_j \right\rangle \right\rangle - \left\langle \left\langle u_i \right\rangle \right\rangle \left\langle \left\langle u_j \right\rangle \right\rangle \tag{16}$$



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Properties

- It is not dissipative enough
- It gives feasible shear stresses (from experience)
- · Logical to combine with Smag. model!



Dynamic approach

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- The idea is the same as in the scale similarity model
- The theory is more complicated
- Any model can be made dynamic
- Dynamic Smagorinsky is widely used (combining the two advantages)



Numerical issues

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- The spatial numerical schemes are used on the border of their capabilities (wave length = cell siez), when $Delta = h \ (h = \text{cell size})$
- The numerical schemes remarkably influence the result
- Grid in-dependency as a function of h/Δ : practically impossible



Boundary Conditions Periodicity

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- · Periodicity is used to model infinite long domain
- The length of periodicity is given by the length scales of turbulence



Boundary Conditions Inlet

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- Much more difficult than in RANS.
- Turbulent structures should be represented
 - Vortices should be synthesized
 - Separate precursor simulation to provide "real" turbulence



Boundary Conditions Wall

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$$y^+ \approx 1 \tag{17}$$

$$e^+ \approx 50$$
 (18)

$$z^+ \approx 10 - 20 \tag{19}$$



Results Time averaged quantities

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- Can be used similarly as results of RANS
- In a lucky situation it is more accurate than the RANS result, in case of bad use can be much more inaccurate



Results Instantaneous structures

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• The movement of the vortices can be tracked

• Enables the control of turbulence



Kérdések

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Thanks for your attention!