

Multiphase and Reactive Flow Modelling

BMEGEÁTMW07

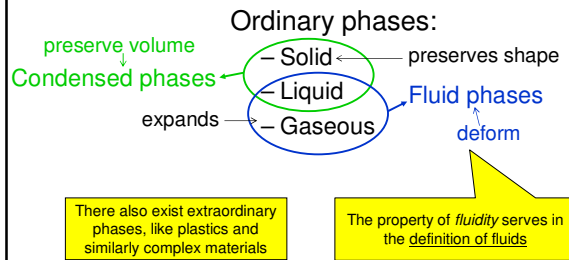
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Basic notions and terminology



Properties and models of solids

Properties of solids:

- Mass (inertia), position, translation → Mass point model
- Extension (density, volume), rotation, inertial momentum → Rigid body model
- Elastic deformations (small, reversible and linear), deformation and stress fields → The simplest continuum model
- Inelastic deformations (large, irreversible and nonlinear), dislocations, failure etc. → Even more complex models

Modelled features:

1. Mechanics
 - Statics: mechanical equilibrium is necessary
 - Dynamics: governed by deviation from mechanical equilibrium
2. Thermodynamics of solids

Models and properties of fluids

Key properties of fluids:

- Large, irreversible deformations
- Density, pressure, viscosity, thermal conductivity, etc. (are these properties or states?)

Features to be modelled:

1. Statics
 - Hydrostatics: definition of fluid (inhomogeneous [pressure and density])
 - Thermostatics: thermal equilibrium (homogenous state)
2. Dynamics
 1. Mechanical dynamics: motion governed by deviation from equilibrium of forces
 2. Thermodynamics of fluids:
 - Deviation from global thermodynamic equilibrium often governs processes multiphase, multi-component systems
 - Local thermodynamic equilibrium is (almost always) maintained

Only continuum models are appropriate!

Modelling Simple Fluids

- Inside the fluid:

– Transport equations

Mass, momentum and energy balances

5 PDE's for $p(t, \vec{r})$, $\vec{u}(t, \vec{r})$ and $T(t, \vec{r})$ → Primary (direct) field variables

– Constitutive equations

Algebraic equations for $\rho(p, T)$, $\mu(p, T)$, $k(p, T)$, ...

- Boundary conditions → Secondary (indirect) field variables

On explicitly or implicitly specified surfaces

- Initial conditions

Thermodynamical representations

Representation (independent variables)	TD potential
entropy and volume ($s, 1/\rho$)	internal energy
temperature and volume ($T, 1/\rho$)	free energy
entropy and pressure (s, p)	enthalpy
temperature and pressure (T, p)	free enthalpy

- All of these are equivalent: can be transformed to each other by appropriate formulae
- Use the one which is most practicable: e.g., (s, p) in acoustics: $s = \text{const} \Rightarrow \rho(s, p) \rightarrow p(p)$.

We prefer (T, p)

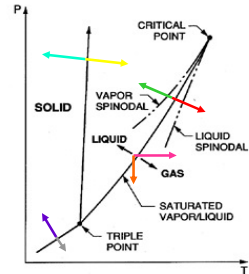
Note

Some models of fluids

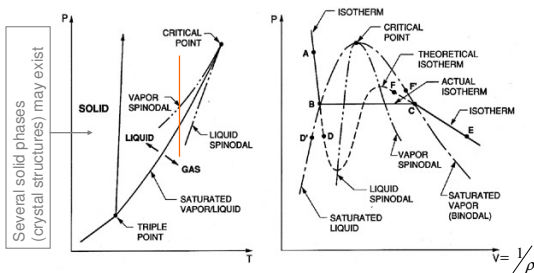
- $\rho = \text{const}, \mu = \text{const}$ → **Stoksean fluid**
- $\rho(p), \mu = \text{const}$ → **compressible (or barotropic) fluid**
In both of these, the heat transport problem can be solved separately (one-way coupling):
 fluid dynamical equations → heat transport equation (1 PDE)
- $\rho(p, T), \mu(p, T), k(p, T), \dots$ → **general simple fluid**
Mutually coupled thermo-hydraulic equations:
 fluid dynamical equations ↔ heat transport equation
- Non-Newtonian behaviour etc. → **models for complex fluids**

Phase transitions

- **Evaporation**, incl.
 - Boiling
 - Cavitation
 - **Condensation**
 - **Freezing**
 - **Melting**
 - **Solidification**
 - **Sublimation**
- All phase transitions involve latent heat deposition or release



Typical phase diagrams of a pure material:



In equilibrium 1, 2 or 3 phases can exist together

Complete mechanical and thermal equilibrium

Conditions of local phase equilibrium in a contact point in case of a pure material

- 2 phases:
 - $T^{(1)} = T^{(2)} =: T$
 - $p^{(1)} = p^{(2)} =: p$
 - $\mu^{(1)}(T, p) = \mu^{(2)}(T, p)$
 - Locus of solution: a line $T_s(p)$ or $p_s(T)$, the **saturation** temperature or pressure (e.g. 'boiling point').
- 3 phases:
 - $T^{(1)} = T^{(2)} = T^{(3)} =: T$
 - $p^{(1)} = p^{(2)} = p^{(3)} =: p$
 - $\mu^{(1)}(T, p) = \mu^{(2)}(T, p) = \mu^{(3)}(T, p)$
 - Locus of solution: a point (T_t, p_t) , the **triple point**.

Multiple components

Almost all systems have more than 1 chemical components

Phases are typically *multi-component mixtures*

- **Concentration(s)**: measure(s) of composition

There are lot of practical concentrations in use, e.g.

– **Mass fraction** (we prefer this!)

$$c_1 = m_1/m, \quad c_2 = m_2/m, \quad \dots \quad c_k = m_k/m, \quad \dots \quad \sum_k c_k = \sum_k m_k/m = 1$$

– **Volume fraction** (good only if volume is conserved upon mixing!)

$$\alpha_1 = V_1/V, \quad \alpha_2 = V_2/V, \quad \dots \quad \alpha_k = V_k/V, \quad \dots \quad \sum_k \alpha_k = \sum_k V_k/V = 1$$

Concentration fields appear as new primary field variables

in the equation: $c_k(t, \vec{r})$ for $k = 2, \dots, N_p$

One of them (usually that of the solvent) is redundant, not used.

Notations to be used (or at least attempted)

- Phase index (upper):
 - (p) or
 - (s), (l), (g), (v), (f) for solid, liquid, gas, fluid, vapour
- Component index (lower): k
- Coordinate index (lower): i, j or t

Examples: $\rho^{(s)}, c_k^{(p)}, u_i^{(p)}$

- Partial differentiation:

$$\partial_t, \partial_i \quad (\partial_1 = \partial_x, \partial_2 = \partial_y, \partial_3 = \partial_z)$$

Note

Material properties in multicomponent mixtures

- One needs constitutional equations for each phase
- These algebraic equations depend also on the concentrations

For each phase (p) one needs to know:

- the equation of state $\rho^{(p)}(p, T, c_1^{(p)}, c_2^{(p)}, \dots)$
- the viscosity $\mu_k^{(p)}(p, T, c_1^{(p)}, c_2^{(p)}, \dots)$
- the thermal conductivity $k^{(p)}(p, T, c_1^{(p)}, c_2^{(p)}, \dots)$
- the diffusion coefficients $D_{k,i}^{(p)}(p, T, c_1^{(p)}, c_2^{(p)}, \dots)$

Conditions of local phase equilibrium in a contact point in case of multiple components

- Suppose N phases and K components:
- Thermal and mechanical equilibrium on the interfaces:
 $T^{(1)} = T^{(2)} = T^{(3)} = \dots = T$
 $p^{(1)} = p^{(2)} = p^{(3)} = \dots = p$
- Mass balance for each component among all phases:

$$\mu_1^{(1)}(T, p, c_1^{(1)}, c_2^{(1)}, \dots, c_K^{(1)}) = \mu_1^{(2)}(T, p, c_1^{(2)}, c_2^{(2)}, \dots, c_K^{(2)}) = \dots = \mu_1^{(N)}(T, p, c_1^{(N)}, c_2^{(N)}, \dots, c_K^{(N)})$$

$$\mu_2^{(1)}(T, p, c_1^{(1)}, c_2^{(1)}, \dots, c_K^{(1)}) = \mu_2^{(2)}(T, p, c_1^{(2)}, c_2^{(2)}, \dots, c_K^{(2)}) = \dots = \mu_2^{(N)}(T, p, c_1^{(N)}, c_2^{(N)}, \dots, c_K^{(N)})$$

$$\vdots$$

$$\mu_K^{(1)}(T, p, c_1^{(1)}, c_2^{(1)}, \dots, c_K^{(1)}) = \mu_K^{(2)}(T, p, c_1^{(2)}, c_2^{(2)}, \dots, c_K^{(2)}) = \dots = \mu_K^{(N)}(T, p, c_1^{(N)}, c_2^{(N)}, \dots, c_K^{(N)})$$

($N-1$) K equations for $2+N(K-1)$ unknowns

Phase equilibrium in a multi-component mixture

Gibbs' Rule of Phases, *in equilibrium*:

$$\# \text{ phases} \equiv N \leq \# \text{ components} + 2 \equiv K + 2$$

TD limit on the # of phases

If there is *no (global) TD equilibrium*:
additional phases may also exist

- in transient metastable state or
- spatially separated, in distant points

Miscibility

The number of phases in a given system is also influenced by the miscibility of the components:

- Gases always mix →
Typically there is at most 1 contiguous gas phase
- Liquids maybe miscible or immiscible →
Liquids may separate into more than 1 phases (e.g. polar water + apolar oil)
 1. Surface tension (gas-liquid interface)
 2. Interfacial tension (liquid-liquid interface)
(In general: Interfacial tension on fluid-liquid interfaces)
- Solids typically remain granular

Topology of phases and interfaces

A phase may be

- *Contiguous*
(more than 1 contiguous phases can coexist)
- *Dispersed*:
 - solid particles, droplets or bubbles
 - of small size
 - usually surrounded by a contiguous phase
- *Compound*

Interfaces are

- 2D interface surfaces separating 2 phases
 - gas-liquid: *surface*
 - liquid-liquid: *interface*
 - solid-fluid: *wall*
- 1D contact lines separating 3 phases and 3 interfaces
- 0D contact points with 4 phases, 6 interfaces and 4 contact lines

Topological limit on the # of phases (always local)

Special Features to Be Modelled

- Multiple components →
 - chemical reactions
 - molecular diffusion of constituents
- Multiple phases → inter-phase processes
 - momentum transport,
 - mass transport and
 - energy (heat) transfer across interfaces.
 (Local deviation from total TD equilibrium is typical)